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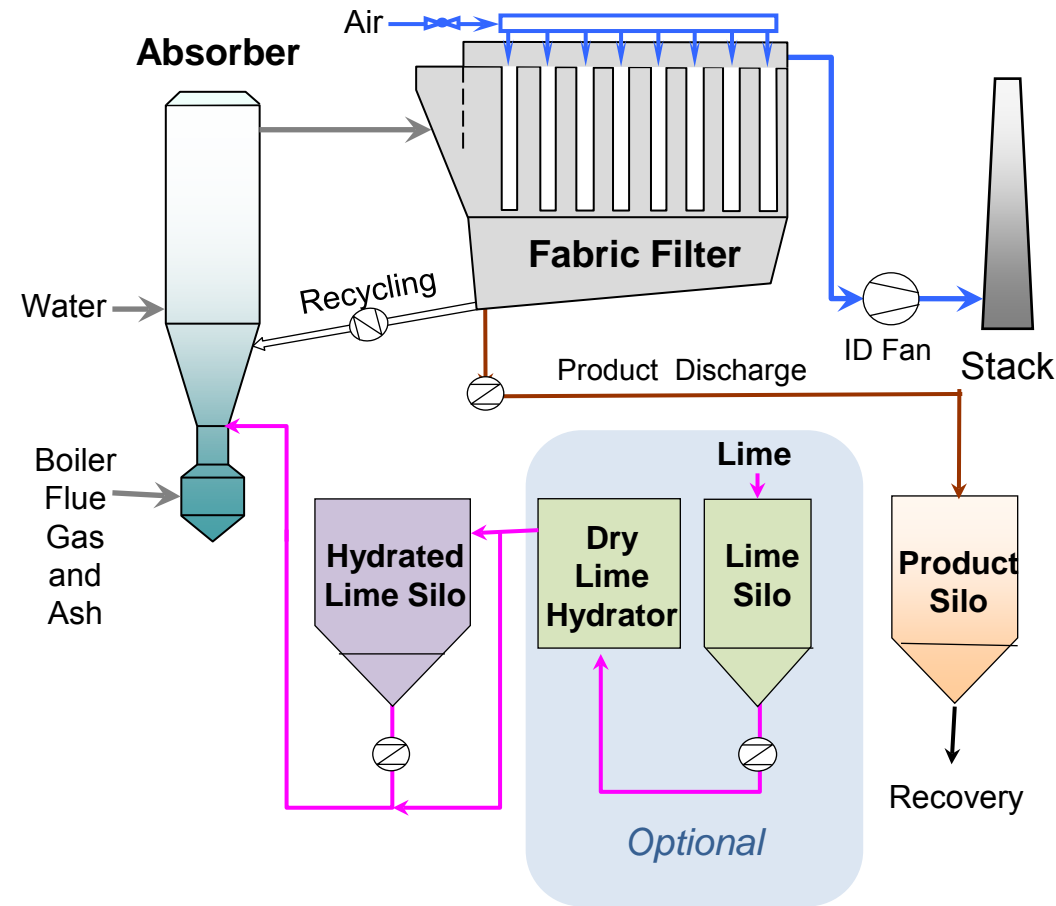
# Circulating Fluidized Bed Scrubbing Technology

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*Rev 071514*

# Circulating Fluidized Bed Scrubbing (CFBS) Technology

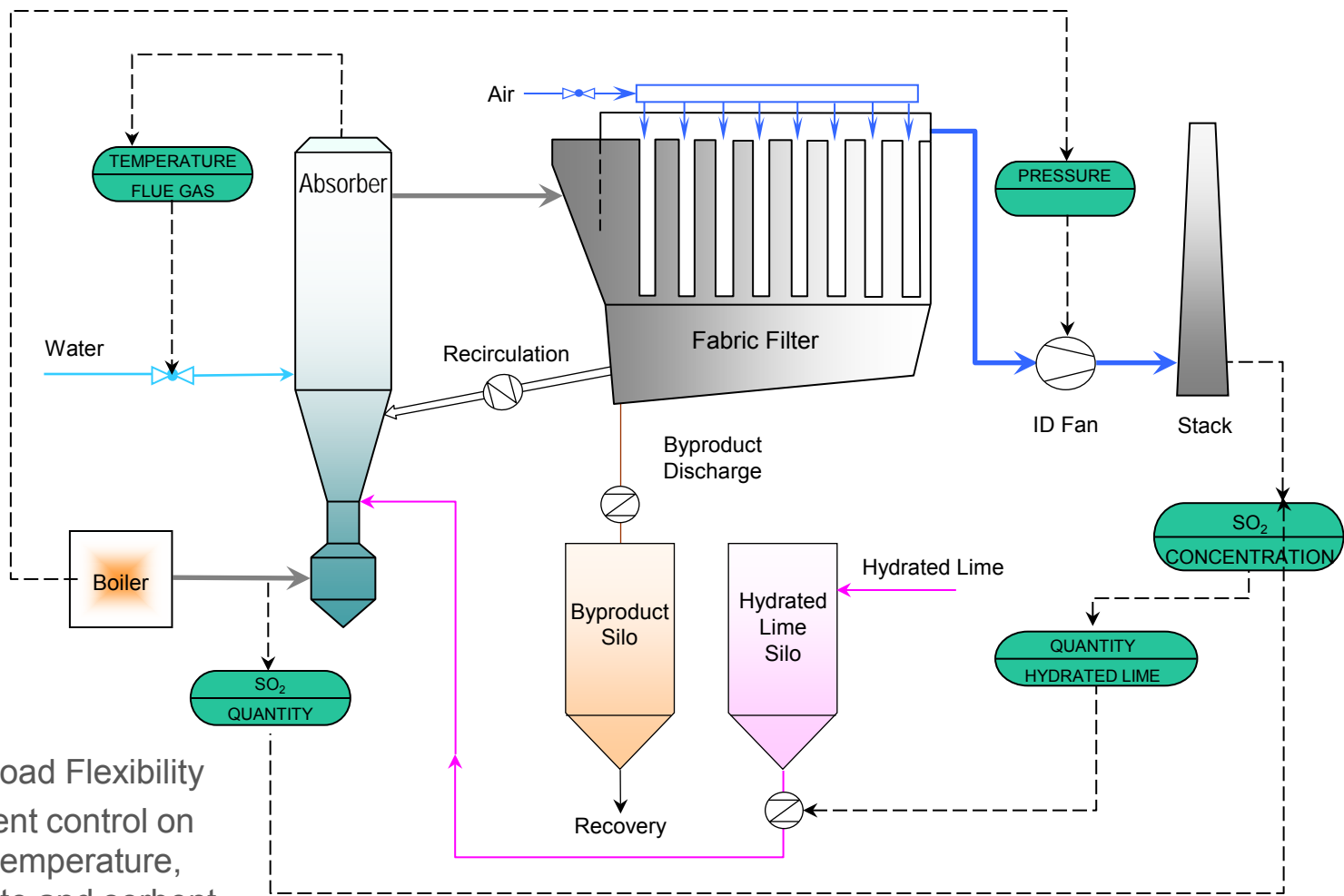


## How does it work?

- Flue gas with or without ash enters the bottom of the absorber, flowing upward through venturi to accelerate the gas flow causing turbulence flow.
- Recycled solids, hydrated lime and water mix with the turbulent flue gas providing gas cooling, reactivation of ash and capture of pollutants.
- The gas and solids enter the baghouse where solids are captured and recycled back to the absorber to capture more pollutants
- Reactive absorbents like activated carbon or others can be added to target specific pollutants
- Optional dry lime hydrator produces hydrated lime on-site from lower cost quick lime

**Flexible, reliable multi-pollutant capture  
with minimal water consumption**

# Independent Reagent and Water Control Provides Widest Capture Range and Minimal Water Need



Fuel and Load Flexibility  
Independent control on  
flue gas temperature,  
recycling rate and sorbent  
injection.

**Essentially, Three (3) Control Loops**

# CFB Scrubber Achieves High Capture of Multiple Pollutants

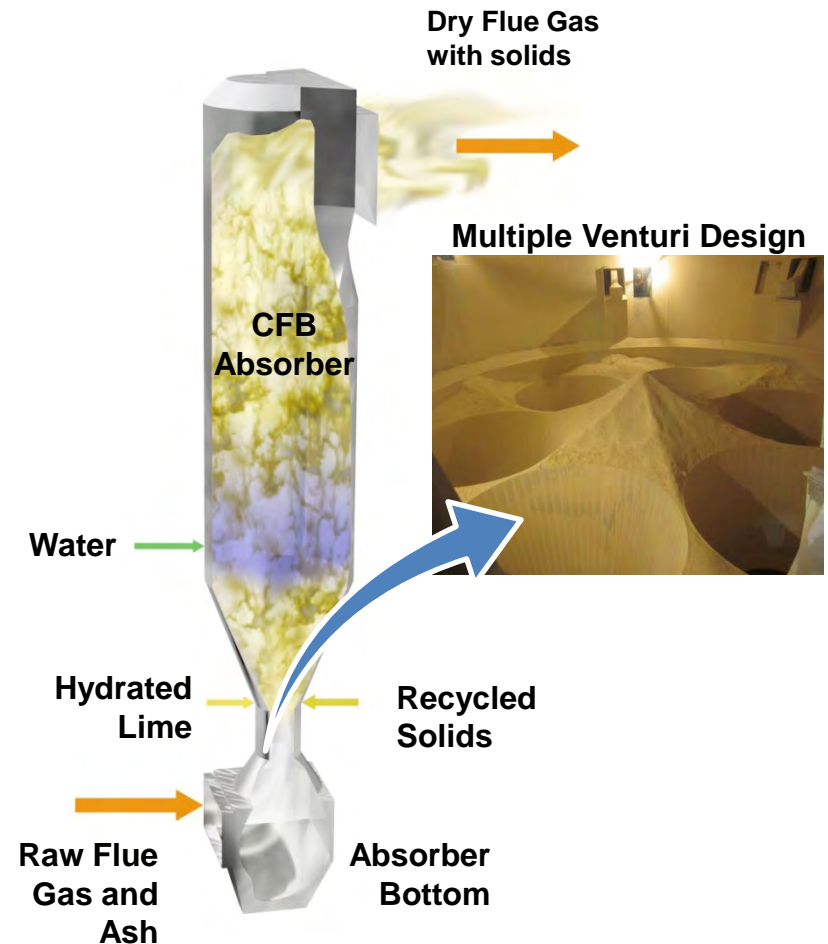
- Typical Performance for Circulating Fluidized Bed Scrubbers

Pollutant	Removal Rate	Notes
SO <sub>2</sub> and SO <sub>3</sub>	Up to 99%	
HCl	85 – 99%	
HF	99%	
Hg <sup>1</sup>	50 – 70%	Low halogen PRB coal – Based on Basin
	80 – 90%	With Eastern Bituminous Fuels (high in Halogens)
	90 – 99%	With Activated Carbon Injection (ACI)
Dioxines, Furanes <sub>1</sub>	95 – 98%	

1) Total of all compounds in all phases expressed as elements

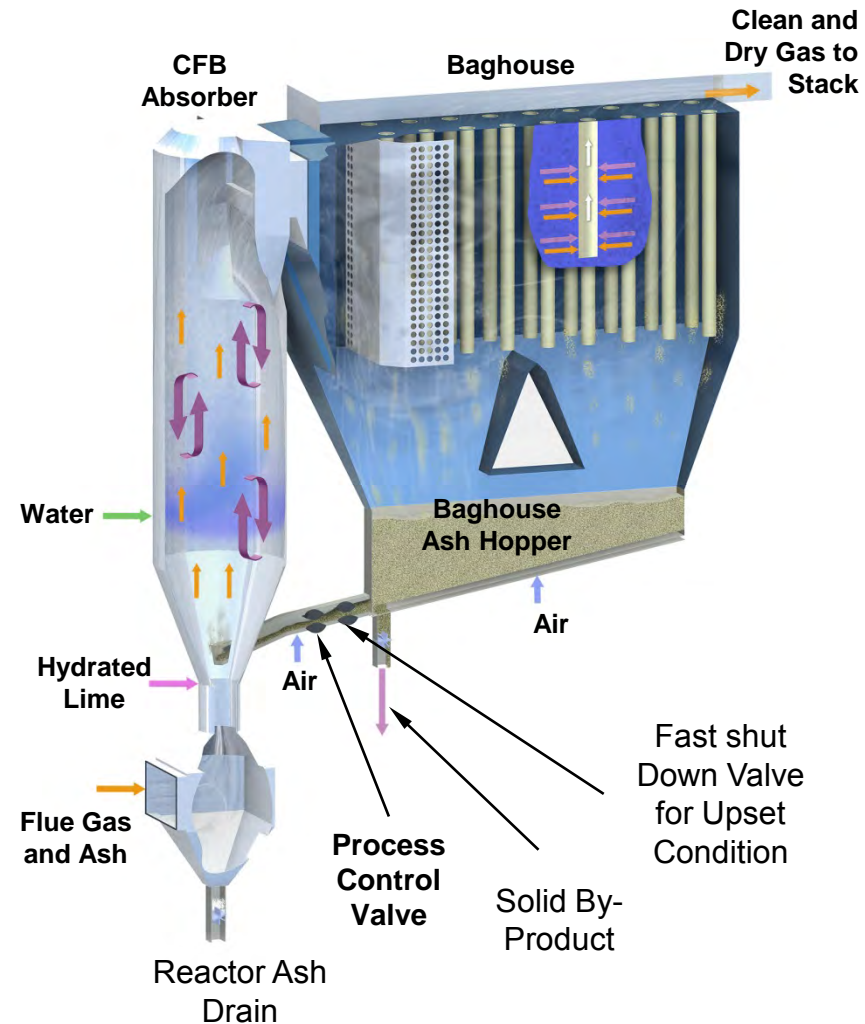
# Design Features of CFB Absorber

- Turbulent CFB absorber provides optimized conditions for multi-pollutant capture
  - Flue gas is efficiently mixed with hydrated lime and water for 4-6 seconds (other single pass technologies have residence times of approximately 1 sec)
  - Wall turbulators increase turbulence near wall
- Flexible process provides wide performance and load range
  - Hydrated lime injection not limited by gas temperature to achieve high pollutant capture
  - Solids and water injected above venturi to ensure high turbulent mixing at low loads
- Low Maintenance
  - No mechanical lime spray heads to maintain
  - Solid circulation keeps reactor surfaces clean
  - Absorber bottom allows easy solids removal for maintenance
  - Low maintenance water nozzles can be replaced while unit is online
- Single absorber designs up to 700 Mwe



# Baghouse and Solid Circulation Design Features

- High Utilization of Sorbents
  - Circulating solids can keep reagents in system up to 20-30 minutes
- Fluidized ash storage in baghouse hopper
- Highly reliable low maintenance air slide
  - No mechanical paddle mixer with their associated maintenance and reliability issues
  - Fast shutdown valve for automatic purging of absorber solids during upset
- Multiple compartment baghouse - typical
  - Low inlet (can) velocity allows high dust loading while maintaining low pulse frequency and long bag life
  - Bag filter cake captures vapor phase metals, acid gases and ammonia slip
- Dry sorbent and product are easy to handle
  - No slurry preparation, handling, dewatering, liquid waste streams
  - Stable dry by-product can be used for land restoration, road base or landfilled

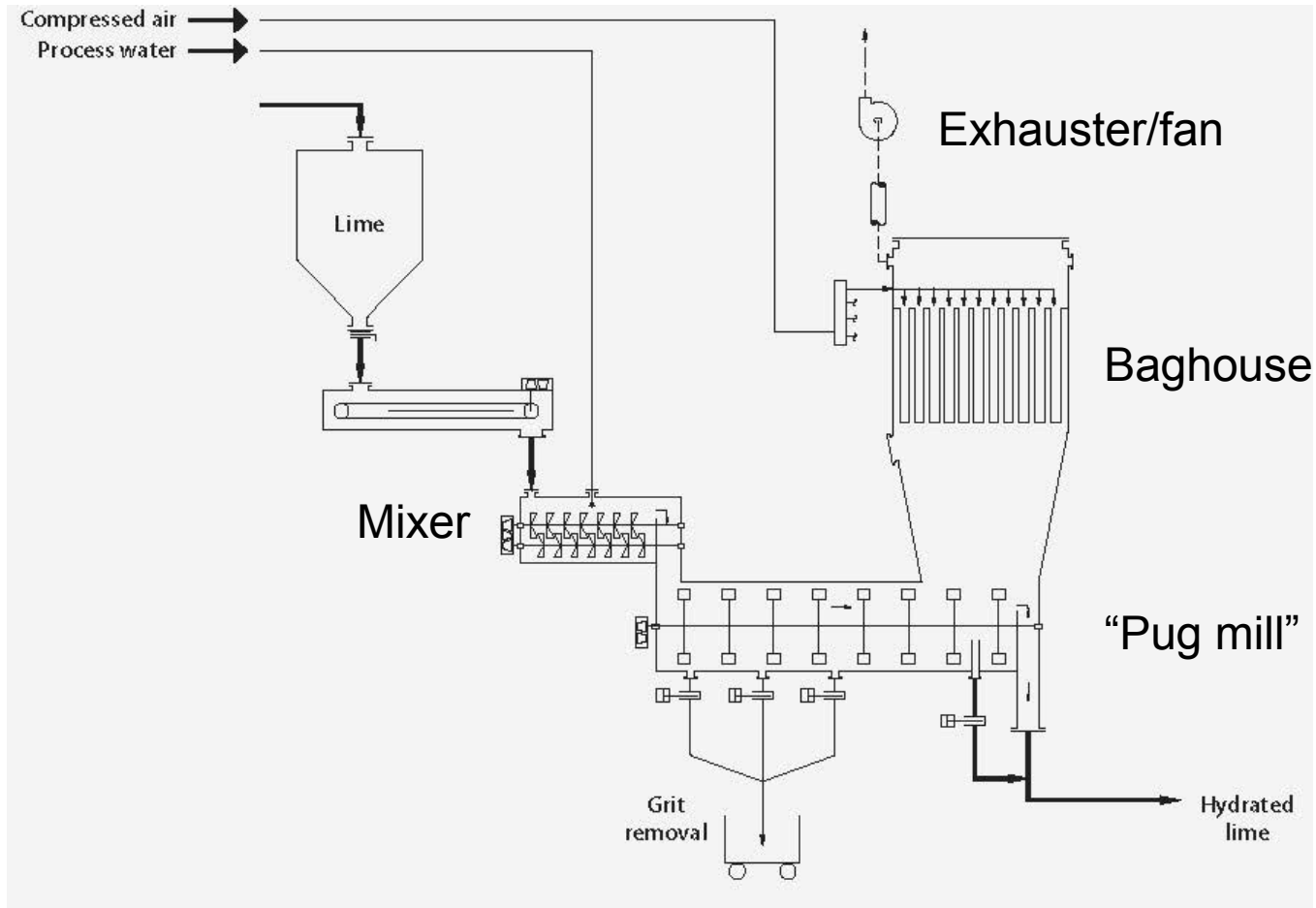


# Lime, Quicklime (CaO), Hydrated Lime (Ca{OH}2) & On-Site Hydration

- “Lime” is a generic term – usually refers to either quicklime or hydrated lime
- Quicklime is produced from the calcination of limestone
- CFBS process requires hydrated lime
  - Direct purchase/injection of Hydrated Lime
  - On-Site Hydration of Lime
- Economic considerations
  - Quicklime is less expensive
  - Δ\$ approximately \$20-30/ton
  - Dependent on location
- On-site hydration

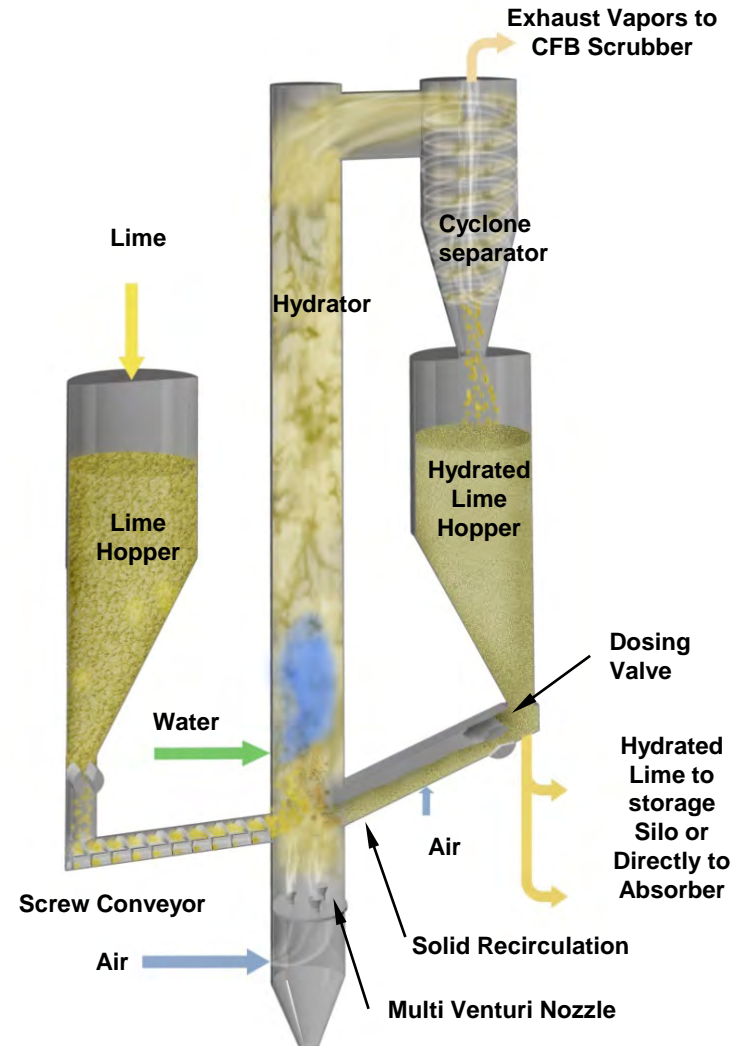


# Mechanical Hydration

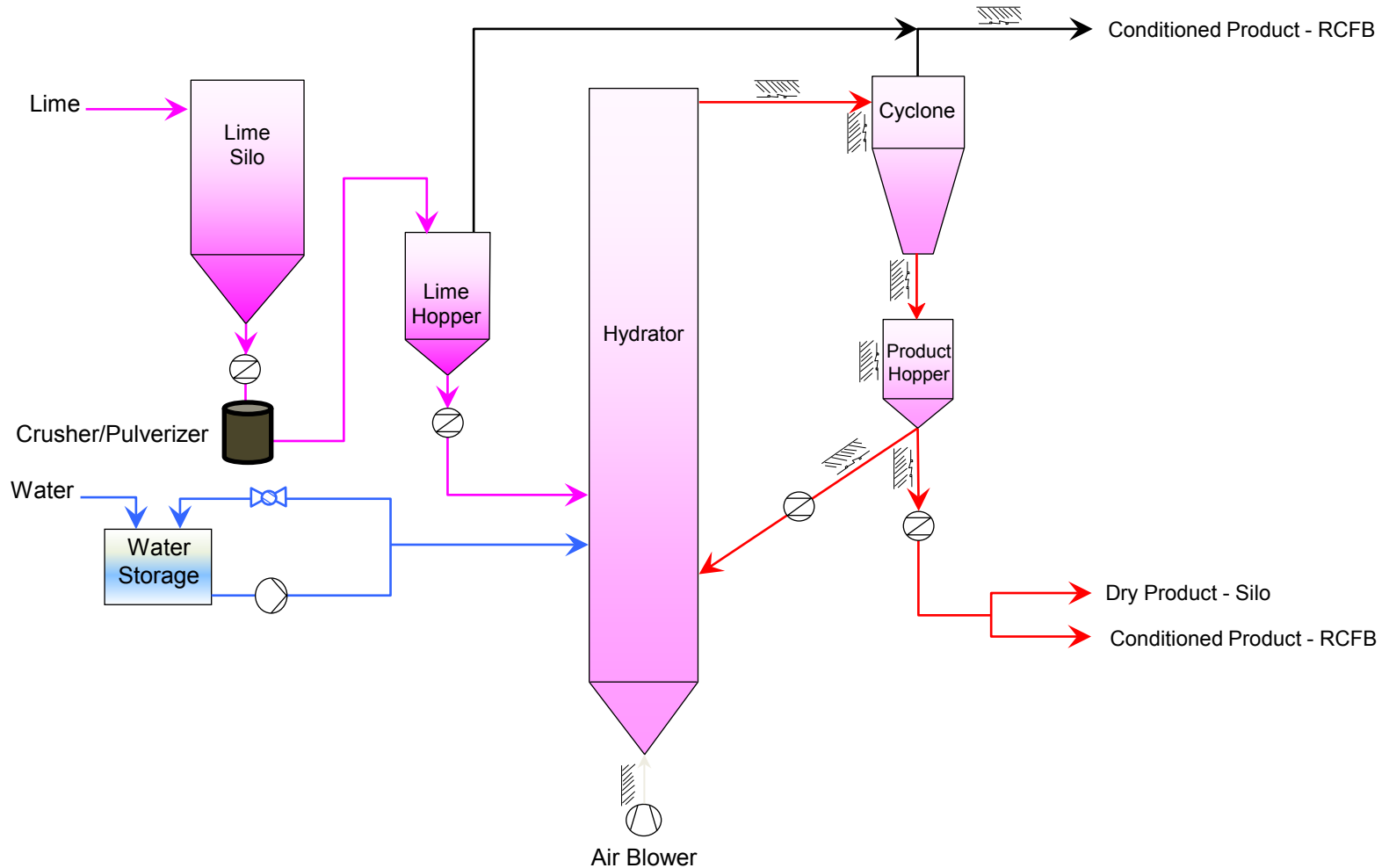


# Fluidized Bed Lime Hydrator

- Produces high quality hydrated lime from economical quick lime
  - High hydrated lime BET surface area improves capture efficiency and lime utilization
- Low maintenance and reliable hydrator
  - No mechanical mixers
  - No rotating parts (except screw conveyor)
  - No slurry handling
  - No exhaust fabric filter or point source emission
- Operational Flexibility Potential
  - Hydrator turn down to 25%
  - Adjustable  $\text{Ca(OH)}_2$  Reactivity Range
    - Higher moisture level when direct feeding to CFB absorber for higher reactivity
    - Lower moisture level for stable silo storage



# Process Diagram of Lime Dry Hydration (LDH) Plant



# Hydrator Differences/Benefits

## Circulated Fluidized Bed Mixing


























- Advantages:
  - homogenized mixing in the fluidization bed
  - stable and continuous operation
  - flexible and adjustable operation parameters if lime quality change
  - continuously produced high quality
  - safe control of hydration rate
  - high reliability and availability due to a minimized use of rotating parts
  - optimized for power plant applications
  - No additional bag filter due to integrated operation concept
  - Hydrator grit transferred to absorber
- Disadvantages:
  - slightly higher energy consumption due to fluidized air, pulverizer/crusher

## Mechanical Mixing

- Advantages:
  - slightly lower energy consumption
  - higher throughputs available
- Disadvantages:
  - agglomeration of material
  - hydration rate difficult to control
  - requires stable lime quality conditions
  - requires intensive operation monitoring
  - requires **frequent** cleaning services
  - higher maintenance for rotating parts (e.g. gears, paddles) required
  - requires additional bag filter for exhaust – **permit source**
  - Impurities (grit) has to be taken out of the mixer frequently

# CFB Scrubber Technology Advantages

## Wet FGD, Spray Dryer FGD, Circulating Fluid Bed FGD

	Wet FGD	SDA FGD	CFB FGD
SO <sub>2</sub> Capture to Meet Low Permit Limits			
Low Water Consumption			
Fuel Flexibility (Fuel Sulfur Variability)			
Fine Particulate Capture			
High SO <sub>3</sub> Capture Efficiency			
Mercury Capture			
Compact System Footprint			
Minimal Maintenance Requirements			
Overall			

Advantage 

Neutral 

Disadvantage 

Source: Basin Electric/Sargent & Lundy Study

# Largest CFB Scrubber is at Dry Fork Station

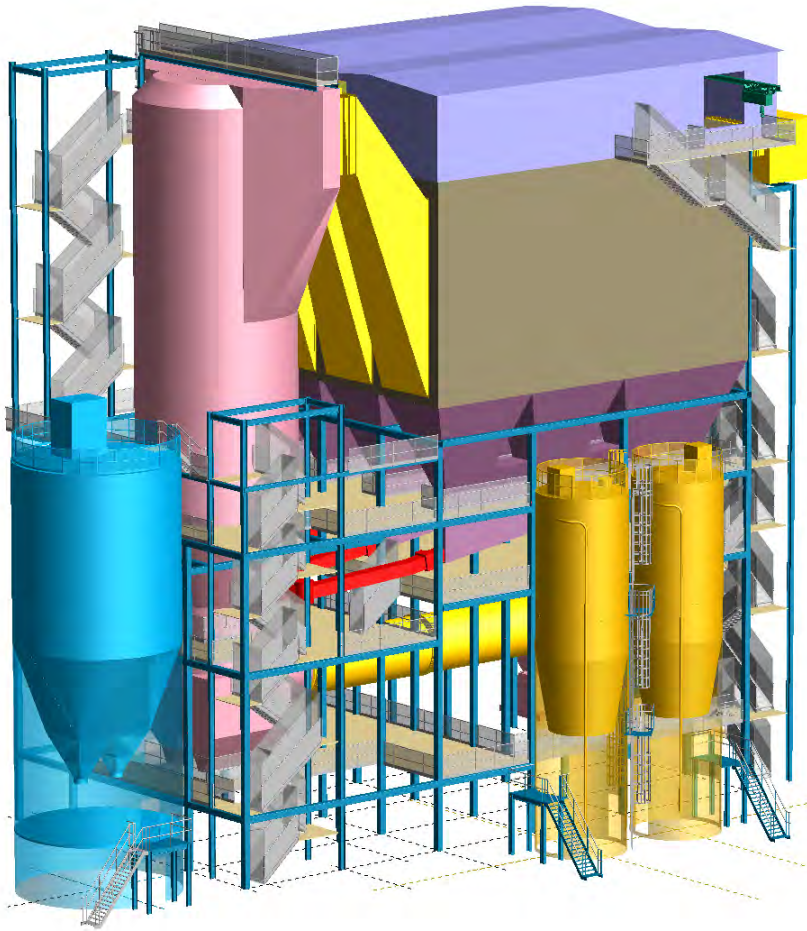
- Plant Location: Gillette, Wyoming, USA
- Plant Elevation ft (m): 4,300 (1,300)
- Customer: Basin Electric Power Cooperative
- Plant Start-Up: June 26, 2011
- Plant Electrical Output: 420 MWe (520 MWe@SL)
- Fuel: PRB Coal
- Scrubber configuration: 1 Reactor, 1 Fabric Filters
- Fuel Sulfur Content: 0.2-0.9% a.r.



Plant MCR Load	Inlet	Outlet	Removal %
Flue gas flow, ACFM (Nm <sup>3</sup> /h)	1,792,000 (1,580,000)	1,550,000(1,690,000)	
SO <sub>2</sub> lb/MMBtu (mg/Nm <sup>3</sup> )	0.30-1.79 (350-2,200)	0.06 (60-75)	80 - 97%
SO <sub>2</sub> ppmv	130-770	20-25	77 - 97%
SO <sub>3</sub> ppmv (mg/Nm <sup>3</sup> )	8-14 (25-42)	0.3-0.6 (1-2)	96%
HCl ppmv (mg/Nm <sup>3</sup> )	5-9 (8-15)	2-3 (4-6)	60 - 67%
Dust lb/MMBtu (mg/Nm <sup>3</sup> )	3-5 (4,000-6,000)	0.012 (12-17)	99.6 - 99.9%
Temperature °F (°C)	294 (146)	155-175 (70-80)	

# On-going Product Development Efforts

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**Foster Wheeler has been active in advancing the technology through R&D efforts**

**Some initiative items include;**

- Hg speciation measurement
- Absorber operational temperature optimization
- Hydrator Optimization
- PAC injection location optimization

# Mercury (Hg) Reduction

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## CFBS has inherent Hg capture capabilities...

- With and without Powder Activated Carbon (PAC) injection
- However it is highly dependent on fuel (halogen content, Hg content, speciation, etc.)
- Injection location considerations
- Hydrator Optimization
- Halogenation
  - PAC
  - Fuel
  - Flue gas

**PAC Consumption can be a significant evaluation factor**

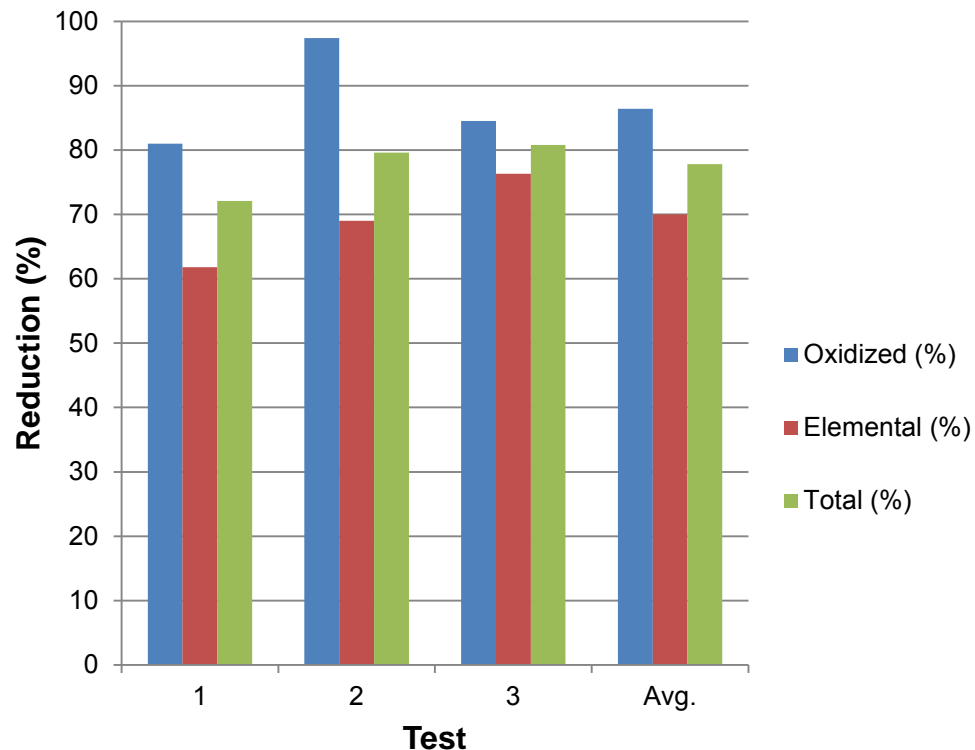
# Mercury Reduction Capabilities

## Foster Wheeler's Hg reduction initiative...

- Several units (PC, CFB)
- Different fuels
- Hg speciation
- PAC injection location

Preliminary Data (at right)  
showing Oxidized, Elemental &  
Total Hg reduction

**NOTE: No PAC injection**



# Absorber Operation Temperature

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The absorber operational temperature is usually referenced to as the *“approach to saturation temperature”*

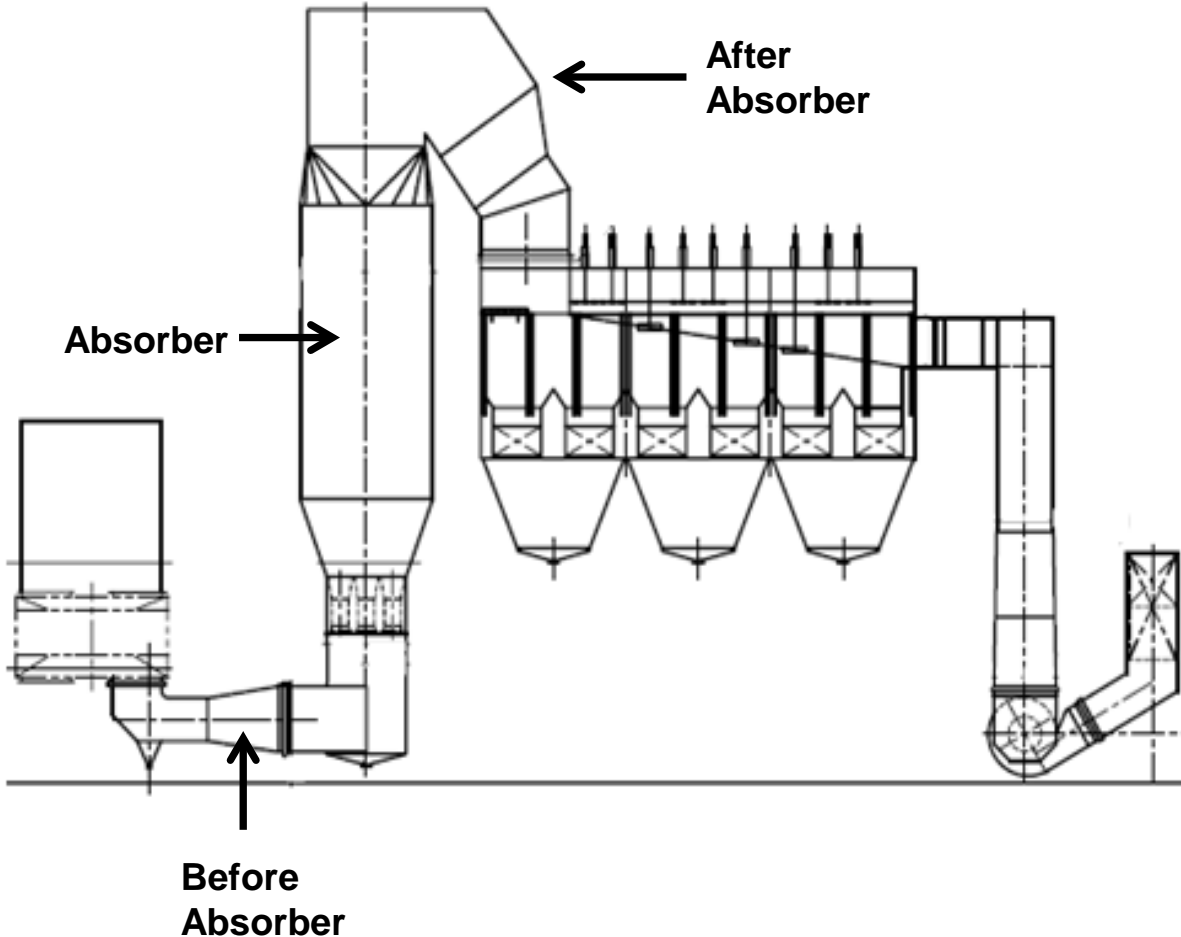
Typically Limited to +30 F

Impacts include:

- Lime Usage (Ca/S)
- Agglomeration/deposits
- Corrosion

Consequently, there are “trade-offs” in operation

# PAC Injection Location



## Before Absorber

High(er) Temperature  
SO<sub>3</sub> Concerns

## In Absorber

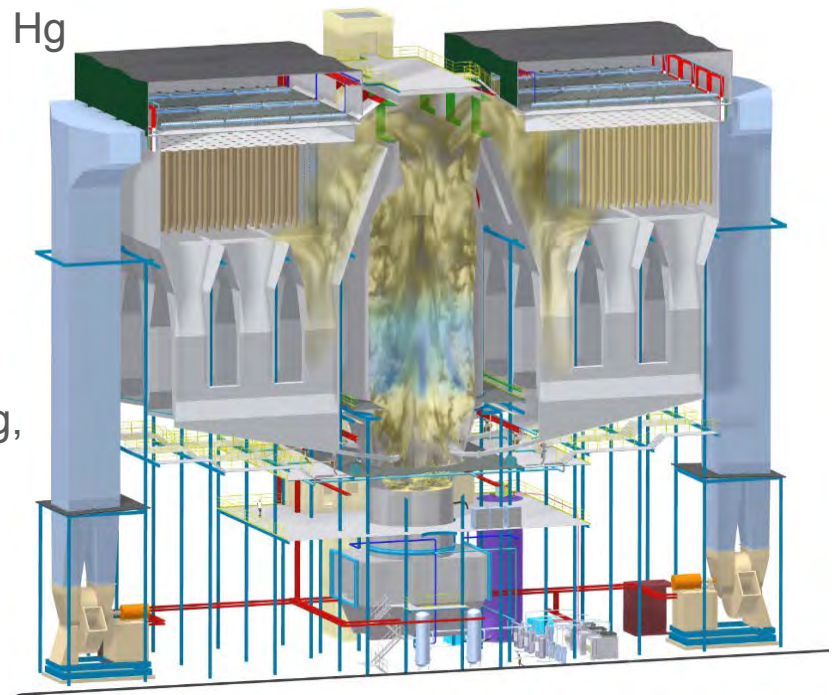
Temperature Lower  
No SO<sub>3</sub> Concerns  
Residence Time Sufficient?

## After Absorber

Temperature Lower  
No SO<sub>3</sub> Concerns  
Residence Time Sufficient?  
Space Available?

# Advantages of CFB Scrubber Technology

- High Multi-Pollutant Capture Capability
  - Up to 99% Capture of SO<sub>2</sub>, SO<sub>3</sub>, HCl, HF, Hg
- Low Installed Cost
  - 50% less than wet FGD
- Low Water Use
  - 30- 40% less than wet FGD
- High Reliability and Low Maintenance
  - No slurry preparation, handling, dewatering, liquid waste streams
  - No mechanical atomizers or spray heads
  - No paddle mixers
- Compact Foot Print
- High Operational Flexibility
  - Capture not limited by flue gas temperature
  - Lower cost lime can be used with Hydrator
  - Ability to use low-quality lime and water



Basin Dry Fork Unit Provides Proven Reference at 525 MWe for SINGLE absorber vessel designs



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**Thank You For Listening**